

Screw Expanders in ORC applications, review and a new perspective

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Re-view: Many shapes and forms





Re-view of Twin Screw Expanders





Re-view: 1960's ORC applications gain momentum

Automotive propulsion

Solar heat + combustion Oil injected Twin Screw

Solar Powered Pumping Stations Off-grid water pumping Oil injected Twin Screw

description

fisbilité. L'enveloppe du moteur renferme outre le corps de détente, le séparateur d'huile, la pompe te le réchauffeur d'huile, Elle contient aussi la pompe à fréon de sort uil in y air qu'un seu passage étanche d'arbre





L'ensemble moteur est bâti autour d'un collaboration avec CIT-ALCATEL. Le moteur à vis est une machine volumérique à base vitesse de rotation 13 000 tr/mm

MOTELAR A VIS SCREW EXPANDER

The motor unit is built on the basis of a screw expander developped with CT-ALCATEL. Screw expander is a volumetric low speed engine (rotating speed is 3.000 r.p.m. for the middle range machinel using low flows (less than 300 r.g. h

in the inlet conditions); its power range runs from 5 to 80 kilowatts. High reliability is obtained with that expander design, been basically composed by two marger

The motor unit contains the expander, oil retainer, oil pump and heater.

It also contains the freon pump in order to have only one shaft seal in the unit.





2-phase expansion modeling?





2-phase expansion modeling?

Physics	Comment	Models	Application
Fluid state conditions	Needed at all positions	Quasi-static	Non quasi-static
Spontaneous condensation	Instable sub-cooled gas	Non-validated (vol, expansion)	Primary impact
Dynamic flashing	Instable super- heated liquid	Non-validated (vol, expansion)	Primary impact
Time constants	Damping effects	Undefined	Differs by order of magnitude
Coupled effects	Condensation/flashi ng interaction	None available	Strongly coupled
Impact of lubricant	Distortion of saturation temp + solubility	Equilibrium models	Strongly time + system dependent



2-phase expansion modeling: ORC system

	Physics based models	Correlation models
Heat exchange	Available	Available
ORC process states	Available	Available
Pump efficiencies	Available	Available
Adiabatic Expansion Efficiency (mixed flow)	Not available	$\psi_{2phase} = \frac{d\eta_{ad}}{dX_{entry}} = -0.15 \cdot \eta_{ad,peak} + 0.09$ $\eta_{ad} (X_{entry}) = \eta_{ad,peak} + \psi_{2phase} \cdot (1 - X_{entry}) \cdot 10$ (Öhman, Lundqvist 2013)
		$[\%\eta_{ad}/10\%X_{inlet}]$





Implications on ORC systems optimizations: Variable expansion entry vapor fraction



Öhman, Lundqvist 2014



New perspectives: Importance of fluid choice?



Simulated ORC for WHR of Marine diesel jacket cooling water (Öhman, Lundqvist 2014) Envelope of optimized efficiency f(Exp, Entry Vapor Fraction) vs. Utilization.

3 different fluids

3 different lumped efficiency classes

FoC Corr is a comparative correlation for real units (Öhman, Lundqvist 2013)



New perspectives: Optimization on vapor fraction?



Sensitivity to Expansion Entry Vapor Fraction on NPO and Cost Efficiency WHR from Pulp factory (Öhman 2011) (R245fa, Utilization=0.75, Reversible Cycle, Irreversible heat transfer)



Conclusions

Physics based "mixed flow" Screw Expander modeling are **not yet suitable** for application performance predictions.

Correlation of "mixed flow" performance allows for ORC systems optimization by process simulation.

The perspective of "Variable Mixed Flow Screw Expander Entry" offers:

- An alternative to trans-/supercritical, Multi-staging and Zeotropic blends
- Opportunities for improved ORC **cost efficiency**



Thank You!

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